

## Module-1:Viscous Flow

# Viscous flow between two parallel plates

(when both plates are in rest)

- To understand the *shear stress distribution*.
- To understand the *velocity distribution* and find out the maximum and average velocity.
- To find out the *pressure drop* for a particular length.

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Consider two fixed plates which are at a distance 't' from each other.

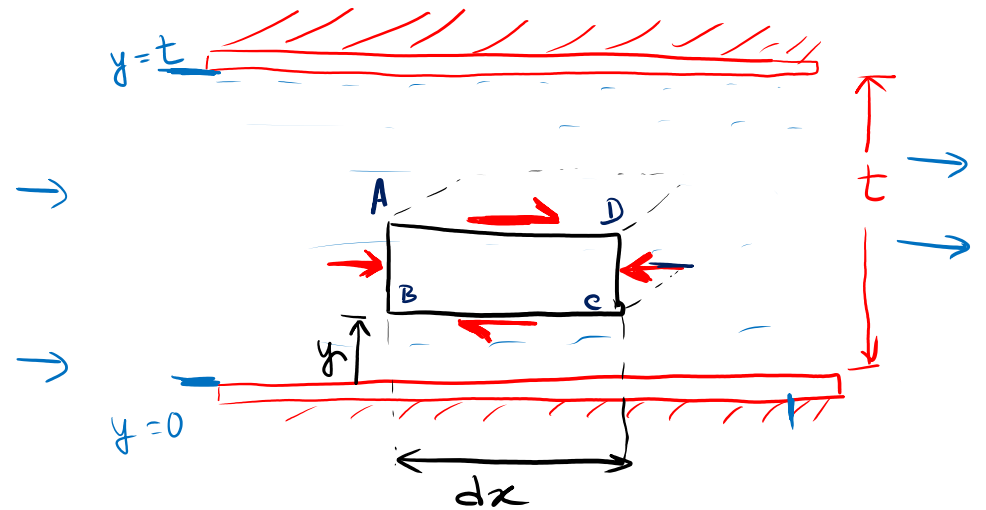
(ABCD)

Consider an element of unit width (=1) at a distance 'y'

from the bottom plate.

$dx$  → length of element

$dy$  → Thickness of element



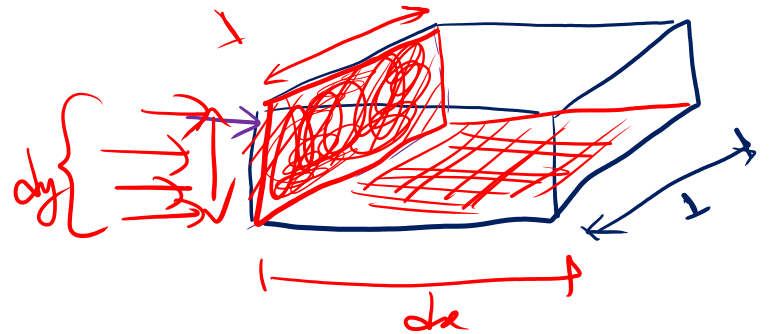
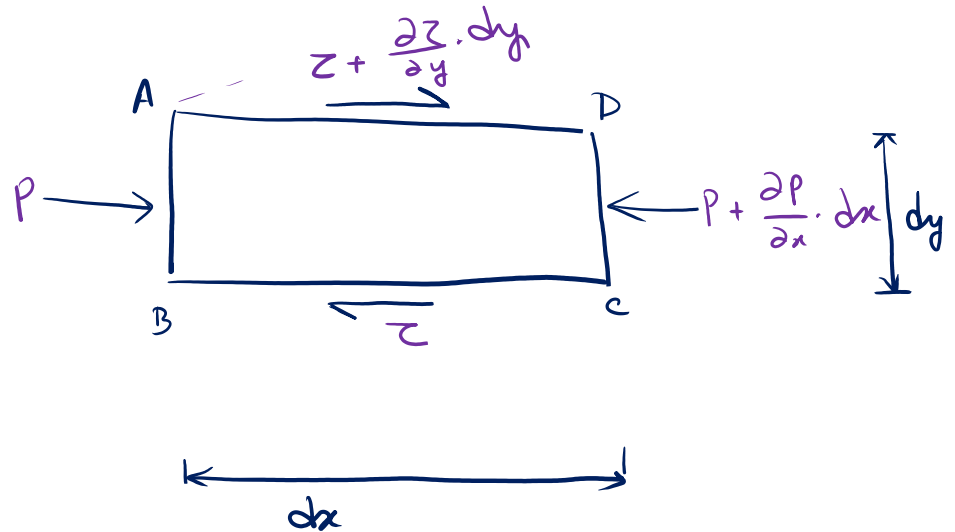
Now, the forces acting on the element are,

$$\textcircled{i} \underline{ON AB} = P \cdot dy \cdot 1 \quad (+ve)$$

$$\textcircled{ii} \underline{CD} = \left( P + \frac{\partial P}{\partial x} \cdot dx \right) \cdot dy \cdot 1 \quad (-ve)$$

$$\textcircled{iii} \underline{BC} = \tau \cdot dx \cdot 1 \quad (-ve)$$

$$\textcircled{iv} \underline{AD} = \left( \tau + \frac{\partial \tau}{\partial y} \cdot dy \right) dx \cdot 1 \quad (+ve)$$



$$P \cdot dy - \left( P + \frac{\partial P}{\partial x} dx \right) \cdot dy - Z \cdot dx + \left( Z + \frac{\partial Z}{\partial y} \cdot dy \right) \cdot dx = 0$$

$$\Rightarrow - \frac{\partial P}{\partial x} dx dy + \frac{\partial Z}{\partial y} \cdot dx dy = 0$$

$$\Rightarrow \boxed{\frac{\partial Z}{\partial y} = \frac{\partial P}{\partial x}}$$

① Velocity distribution

$$Z = \mu \cdot \frac{\partial u}{\partial y}$$

$$\frac{\partial Z}{\partial y} = \frac{\partial P}{\partial x}$$

$$\Rightarrow \frac{\partial}{\partial y} \left( \mu \frac{\partial u}{\partial y} \right) = \frac{\partial P}{\partial x}$$

$$\Rightarrow \frac{\partial^2 u}{\partial y^2} = \frac{1}{\mu} \frac{\partial P}{\partial x}$$

Integrating,

$$\Rightarrow \frac{\partial u}{\partial y} = \frac{1}{\mu} \frac{\partial P}{\partial x} \cdot y + C_1$$

$$\Rightarrow u = \frac{1}{\mu} \cdot \frac{\partial P}{\partial x} \cdot \frac{y^2}{2} + C_1 \cdot y + C_2 \rightarrow \textcircled{1}$$

Applying boundary condition,

$$y=0, u=0, \textcircled{1} \Rightarrow 0 = C_2$$

$$y=t, u=0, \textcircled{1} \Rightarrow 0 = \frac{1}{\mu} \frac{\partial p}{\partial x} \cdot \frac{t^2}{2} + C_1 \cdot t + 0$$

$$\Rightarrow C_1 = \frac{1}{2\mu} \left( -\frac{\partial p}{\partial x} \right) \cdot t$$

Hence,

$$\textcircled{1} \Rightarrow u = \frac{1}{2\mu} \frac{\partial p}{\partial x} \cdot y^2 + \frac{1}{2\mu} \left( -\frac{\partial p}{\partial x} \right) \cdot t \cdot y$$

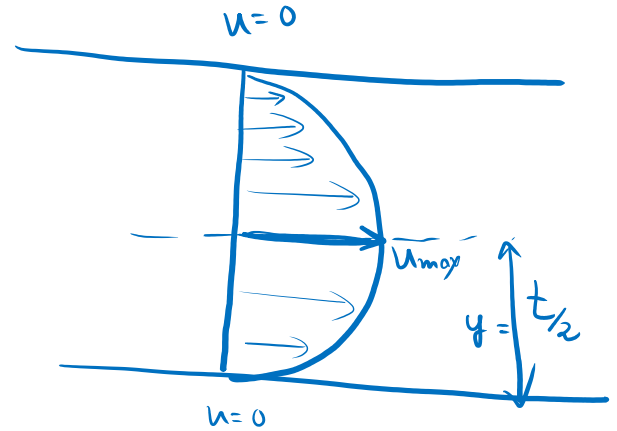
$$u = \frac{1}{2\mu} \left( -\frac{\partial p}{\partial x} \right) [ty - y^2]$$

Max<sup>m</sup> velocity

$$y = \frac{t}{2},$$

$$u_{max} = \frac{1}{2\mu} \left( -\frac{\partial p}{\partial x} \right) \cdot \left[ t \cdot \frac{t}{2} - \left( \frac{t}{2} \right)^2 \right]$$

$$u_{max} = \frac{1}{8\mu} \left( -\frac{\partial p}{\partial x} \right) t^2$$



Avg. velocity ( $\bar{u}$  or  $u_{avg}$ )

$$dQ = u \cdot (dy \cdot 1)$$

$$= \frac{1}{2\mu} \left( -\frac{\partial p}{\partial x} \right) \cdot [ty - y^2] \cdot dy$$

$$\int_0^t dy = \frac{1}{2\mu} \left( -\frac{\partial P}{\partial x} \right) \int_0^t (ty - y^2) dy$$

$$= \frac{1}{2\mu} \left( -\frac{\partial P}{\partial x} \right) \cdot \left[ \frac{t \cdot y^2}{2} - \frac{y^3}{3} \right]_0^t$$

$$Q = \frac{1}{12\mu} \left( -\frac{\partial P}{\partial x} \right) \cdot t^3$$

$$u_{avg} = \frac{Q}{A} = \frac{Q}{t}$$

$$u_{avg} = \frac{1}{12\mu} \cdot \left( -\frac{\partial P}{\partial x} \right) \cdot t^2$$

✓



## Ratio of max & avg velocity

$$\frac{U_{\max}}{U_{\text{avg}}} = \frac{1/8}{1/12} = 1.5$$

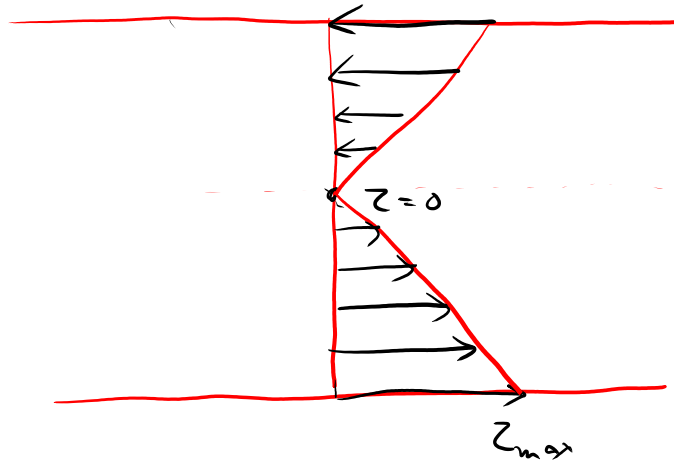
$$U_{\max} = 1.5 U_{\text{avg}}$$

## Shear stress

$$\tau = \mu \cdot \frac{\partial u}{\partial y}$$

$$= \mu \cdot \frac{\partial}{\partial y} \left[ \frac{1}{2\mu} \left( -\frac{\partial P}{\partial x} \right) (t_y - y^2) \right]$$

$$\tau = \frac{1}{2} \cdot \left( -\frac{\partial P}{\partial x} \right) (t - 2y) \rightarrow \underline{\underline{\text{linear variation of shear stress}}}$$



$$y = 0, \quad \tau_{max} = \frac{1}{2} \left( -\frac{\partial P}{\partial x} \right) \cdot t$$

$$y = t, \quad \tau_{max} = \frac{1}{2} \left( -\frac{\partial P}{\partial x} \right) \cdot (-t)$$

$$y = \frac{t}{2}, \quad \tau_{min} = 0$$

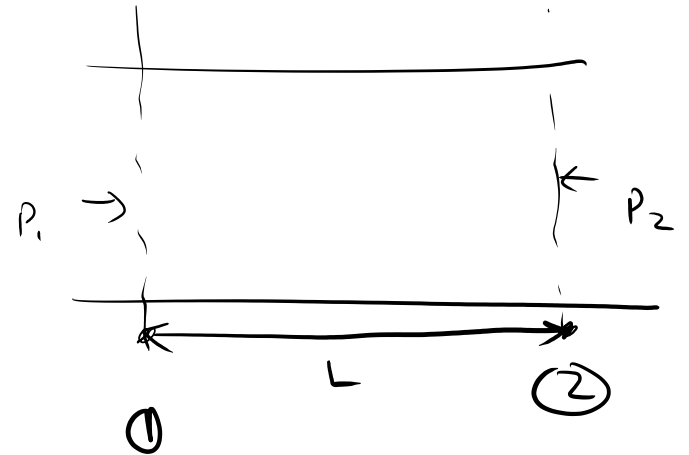
⊗ Pressure drop bet<sup>n</sup> two points at a dist 'L' apart:

$$U_{avg} = \frac{1}{12\mu} \left( -\frac{\partial P}{\partial x} \right) \cdot t^v$$

$$\Rightarrow \left( -\frac{\partial P}{\partial x} \right) = \frac{12 \cdot \mu \cdot U_{avg}}{t^v}$$

$$\Rightarrow \int_{P_1}^{P_2} -\partial P = \frac{12 \mu U_{avg}}{t^v} \int_0^L \partial x$$

$$\Rightarrow \boxed{P_1 - P_2 = \frac{12 \mu \cdot U_{avg} \cdot L}{t^v}}$$



$$\boxed{\frac{P_1 - P_2}{\rho g} = \frac{12 \mu \cdot U_{avg} \cdot L}{\rho g t^v}}$$

**Q.3** Calculate (i) pressure gradient along the flow, (ii) average velocity and discharge of oil of viscosity 0.02 N.s/m<sup>2</sup> flowing between two parallel stationary plates 1 m wide maintained 10 mm apart. Velocity at midway between the plates is 2 m/s

Soln

$$\mu = 0.02 \text{ N.s/m}^2$$

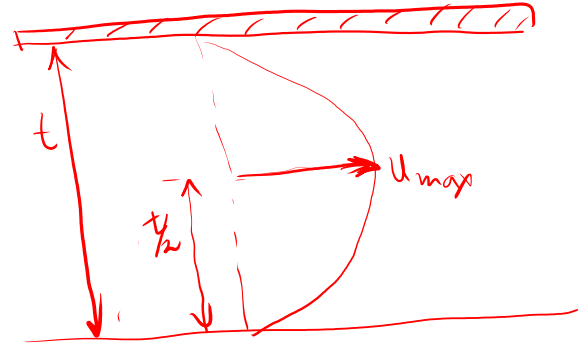
$$t = 10 \text{ mm} = 0.01 \text{ m}, \quad B = 1 \text{ m}$$

$$u_{\text{max}} = 2 \text{ m/s}$$

$$\left( \frac{-\partial P}{\partial x} \right) = ?$$

$$u_{\text{avg}} = ? \quad \checkmark$$

$$Q = ? \quad \checkmark$$



$$\textcircled{1} \quad \frac{u_{\text{max}}}{u_{\text{avg}}} = 1.5$$

$$\Rightarrow u_{\text{avg}} = \frac{2}{1.5} = \frac{4}{3} \text{ m/s} = 1.33 \text{ m/s}$$

$$\textcircled{2} \quad Q = u_{\text{avg}} \times A = \frac{4}{3} \times (0.01 \times 1) = 0.0133 \text{ m}^3/\text{s}$$

$$u_{\text{avg}} = \frac{1}{12\mu} \left( -\frac{\partial p}{\partial x} \right) \cdot t^{\nu}$$

$$\Rightarrow -\frac{\partial p}{\partial x} = \frac{12\mu \cdot u_{\text{avg}}}{t^{\nu}} = \frac{12 \times 0.02 \times \frac{4}{3}}{1^{\nu}} = 0.32 \text{ N/m}^3$$
$$= 0.32 \text{ N/m}^2/\text{m}$$

***Try Solving some more numericals to  
improve yourself.***

***Thank you.***